

# **Slipstream Development & Testing of Post- Combustion CO<sub>2</sub> Capture and Separation Technology for Existing Coal-Fired Plants**

**DOE Contract DE-FE0003714**

**John L Winkler, Siemens**

**2.5 MWe Slipstream utilizing Siemens Amino  
Acid Salt (AAS) Solvent PostCap**

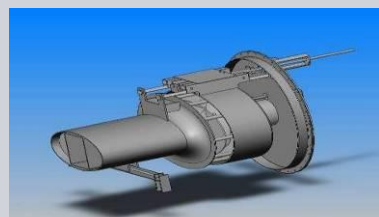
**NETL CO<sub>2</sub> Capture Technology Meeting, August 23, 2011**

# Siemens Energy, Inc.

## Environmental Systems & Services

### Expanded Products for Global Markets

**SIEMENS**



- **Carbon Capture Technology (CC)**
  - Siemens PostCap Process
- **Flue Gas Desulfurization (FGD)**
  - Dry FGD
  - Mercury Control
  - Wet FGD
  - Wet ESP
- **Electrostatic Precipitators (ESP)**
  - HaRDE
  - VIGR
- **Fabric Filters (FF)**
  - Pulse Jet
  - Cartridge
  - Reverse Air
- **NO<sub>x</sub> and Ancillary Products**
  - Low NO<sub>x</sub> Burners
  - Overfire Air
  - SNCR/SCR
  - Boiler Design Upgrades



**steinmüller**  
engineering

**Over 350 Systems & 115,000 MW of Utility Applications**

Siemens Energy, Inc / Energy Sector / Service Division / Environmental Systems  
and Services

## **Project Overview – Project Participants**

- **DOE NETL – Project Sponsor / Awarding Agency**
- **Siemens Energy, Inc. – Technology, Equipment, and Installation provider. Co-Sponsor**
- **Tampa Electric Company – Proposed Host Site Provider, Big Bend Plant Units 1&2**

## Project Objectives


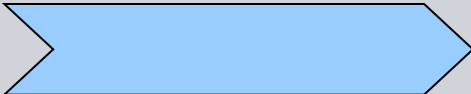

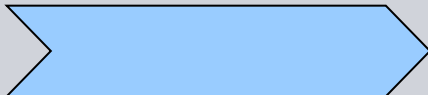

- Demonstrate the ability of POSTCAP technology to achieve 90% CO<sub>2</sub> removal and approach a 35% increase of cost of electricity produced.
  - **AAS technology can reach 90% CO<sub>2</sub> removal (already proven)**
  - **Challenge of approaching 35% increase in COE**
- Demonstrate the scalability and feasibility of progressing the POSTCAP technology to full-scale commercial application (550 MW) on post-combustion CO<sub>2</sub> capture for coal fired power plants and to full-scale commercial application for industrial sources of CO<sub>2</sub> emissions.
  - **Proving scalability**
  - **Proving feasibility**



# Project Overview – Overall Project Performance Dates

Award, October 1, 2010



Activity	
Kick-off	 October 1, 2010
Phase 1 – Process Design	October 1, 2010 <span style="color: red;">October 31, 2011</span> 
Phase 2 – Procurement & Erection	<span style="color: red;">October 31, 2011</span> Aug 31, 2012 
Phase 3 – Operation & Testing	Sept 1, 2012 Jul 1, 2013 
Issue Final Report (draft)	Jul 31, 2013 

## Project Scope

### Slipstream Project Work

- Preliminary Engineering – Phase1
- Detailed Engineering & Design (three month extension) - Phase1
- Development of Equipment/Procurement Packages (three month extension) - Phase1
- Retrofit installation into existing Big Bend scrubber outlet – Phase2
- Commissioning, Operation and Testing of plant – Phase3
- Data Analysis, Report out – Phase3
- Decommissioning/Dismantling



## Project Overview - Funding

	Budget Period 1 Process Design Oct 2010 – <b>Oct 2011</b>		Budget Period 2 Procurement & Erection Oct 2011 – Aug 2012		Budget Period 3 Operation & Testing Sep 2012 – Oct 2013	
	DOE share	Siemens share	DOE share	Siemens share	DOE share	Siemens share
Split (80/20) over 13 qtrs	\$1,411 K	\$353 K	\$10,580 K	\$2,645 K	\$3,008 K	\$752 K
DOE Project Share Total						<b>\$15,000 K</b>
Siemens Project Share Total						<b>\$ 3,750 K</b>

# Status Report – Phase I, Detail Design and Engineering



## Challenges:

- significant underground obstructions found in the area of the proposed plant
- problems in developing steam supply for desorption column
- resulting engineering delays and inefficiencies

## Result:

- Three month extension granted to Phase 1 portion of project schedule by DOE
- Additional costs incurred by Siemens for engineering



# Project Milestones

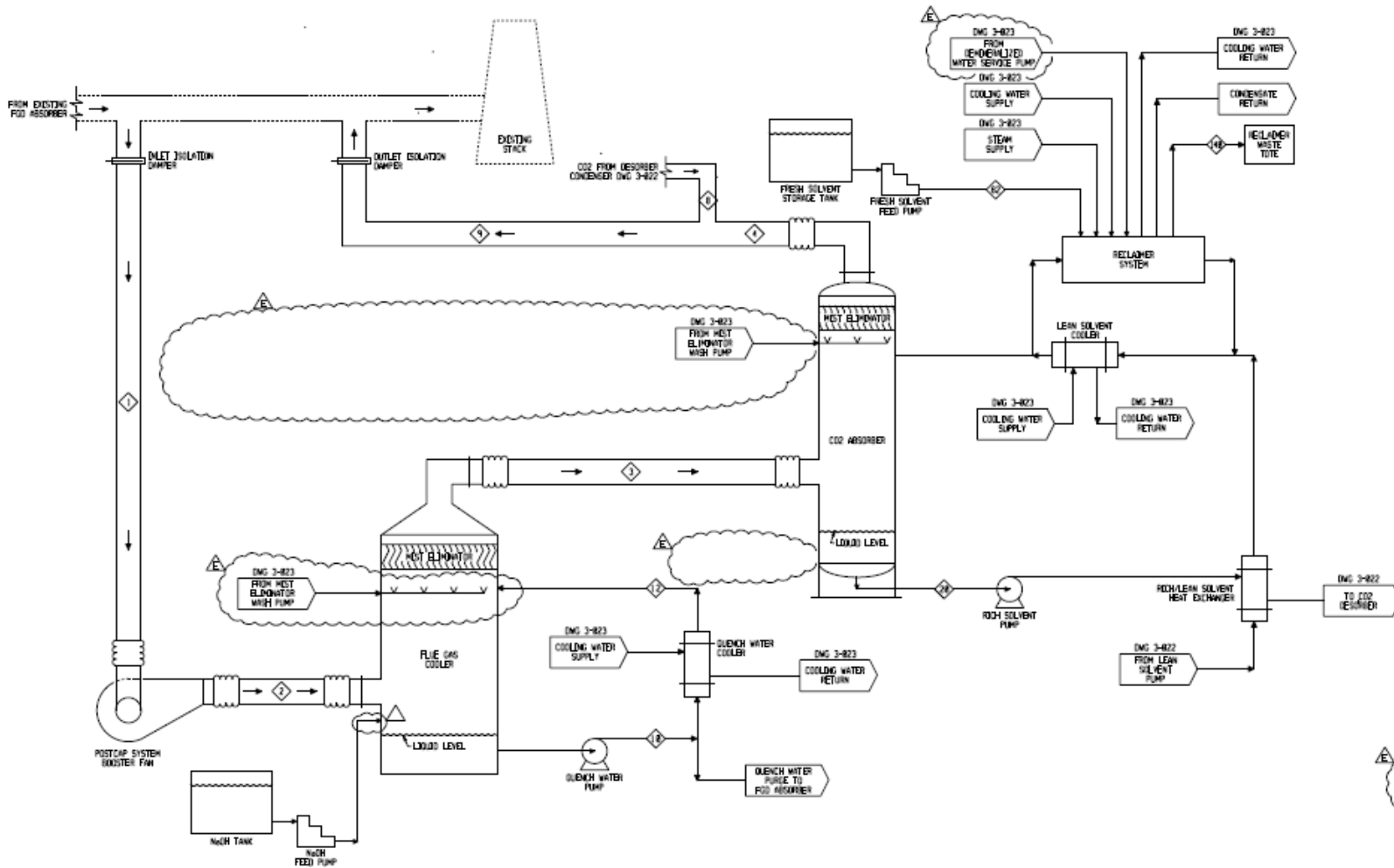
Activity ID	Activity Name	(*)Early Start	(*)Early Fin	Actual Finish
<b>PHASE 1</b>				
SE0900	Task 1.0 Project Management and Planning	10/1/2010	7/31/2011	10/31/2011
SE1012	Task 2.0 Generation of Heat & Material Balance	10/1/2010	11/30/201	
SE1013	Task 3.0 Generation of PFD's	10/1/2010	11/30/201	
SE1014	Task 4.0 Plant Interface Engineering	10/1/2010	6/30/2011	
SE1015	Task 5.0 Preliminary Design	10/1/2010	2/28/2011	
SE1045	Task 6.0 Detail Design	3/1/2011	7/31/2011	10/31/2011

# Project Methodology

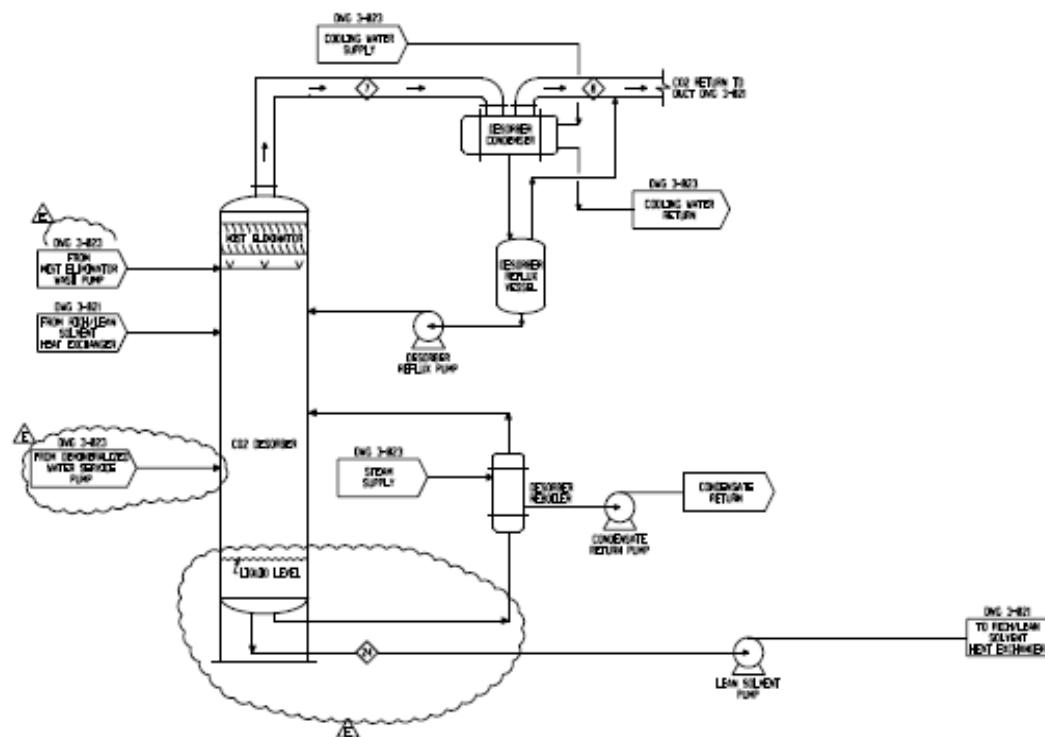
## Schedule

Task 1.0 Preliminary Design Engineering	10/1/2010	2/28/2011
Task 2.0 Generation of Heat & Material Balance	10/1/2010	11/30/2011
Task 3.0 Generation of PFD's	10/1/2010	11/30/2011
Task 4.0 Plant Interface Engineering	10/1/2010	6/30/2011
Task 5.0 Preliminary Design	10/1/2010	2/28/2011
Task 6.0 Detail Design/Engineering	3/1/2011	10/31/2011
Task 7.0 Site Civil Work	8/1/2011	11/31/2011
Task 8.0 Plant Equipment & Material Procurement	8/1/2011	8/30/2012
Task 9.0 Complete Erection of Structural Steel	9/1/2011	2/15/2012
Task 10.0 Absorber/Desorber Installation Complete	9/1/2011	5/9/2012
Task 11.0 Mechanical Installation Complete	9/1/2011	5/9/2012
Task 12.0 Piping Component Installation	12/1/2011	8/30/2012
Task 13.0 Complete Electrical Installation	2/1/2012	7/13/2012
Task 14.0 Complete I&C Installation	2/1/2012	8/30/2012
Task 15.0 Test Plan Development	6/1/2012	8/31/2012
Task 16.0 Phase 3 - Commissioning, Testing, and Reporting	9/1/2012	7/31/2013
Task 17.0 Perform System Hydro Test	9/1/2012	10/1/2012
Task 18.0 Perform Plant Startup	10/31/2012	12/3/2012
Task 19.0 Steady State Plant Operation	12/3/2012	7/1/2013
Task 20.0 Perform Testing	12/3/2012	7/1/2013
Task 21.0 Data Analysis	7/2/2013	7/31/2013
Task 22.0 Decommission	8/1/2013	10/31/2013
Task 23.0 Disassemble	8/1/2013	10/31/2013

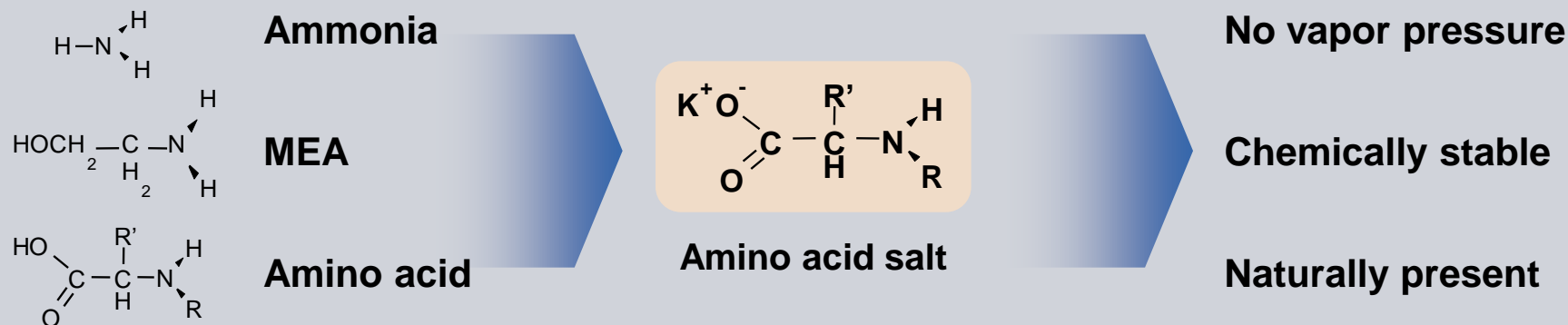
# POST CAP PFD (1 of 2)



## POST CAP PFD (2 of 2)



# Technology Fundamentals – Amino Acid Salt is the basis of our solvent



## Salts have no vapor pressure

- No thermodynamic solvent emissions
- Not flammable
- Not explosive
- Odorless
- No inhalation risk



## Negative ion is less sensitive to O<sub>2</sub>

- Low degradation

## Amino acids are naturally present

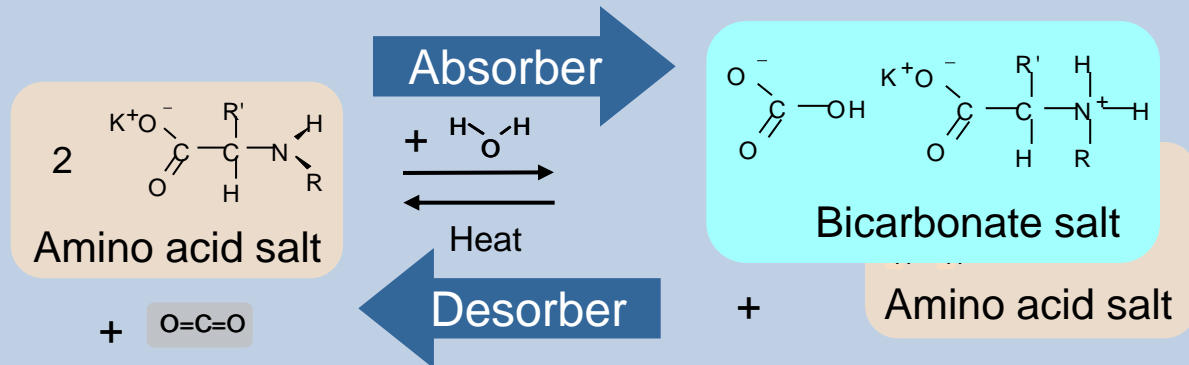
- Biodegradable
- Nontoxic
- Environmentally friendly



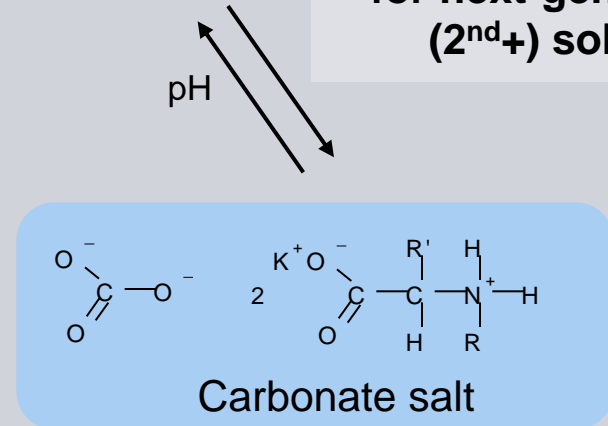
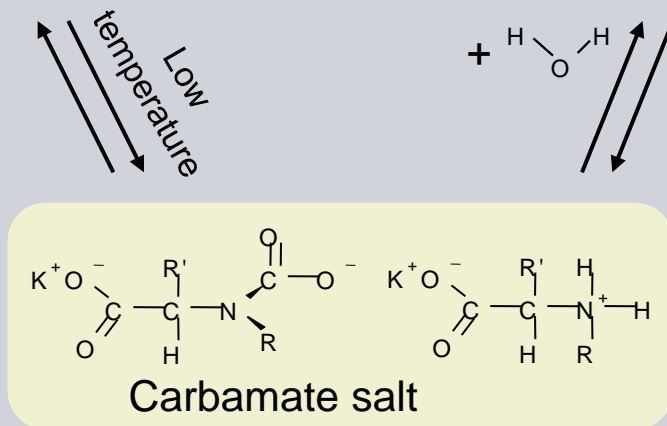


# Technology Fundamentals

Preferred reaction mode



**Precipitation is an option for next-generation (2<sup>nd</sup>+) solvent**



Intermediate reaction products fulfill the same HSE standard as amino acid salts

# Technology Background - Solvent Stability and Current Performance

Components	Amino Acid Salt w/o H <sub>2</sub> O wash
VOC	not detectable
Formaldehyde	not detectable
Methylamine	not detectable
ΣNitrosamines	not detectable
Ammonia	<1 ppm

- the solvent is highly stable and does not lead to measurable loss of active substance due to degradation
- by-products in the liquid phase are salts with no vapor pressure
- No production of any mentionable amounts of emissions
- small amounts of heat stable salts (HSS) and nitrosamines will be removed with reclaimers

The amino-acid salt is stable against thermal stress and oxygen environments

# Background - Siemens lab plant for CO<sub>2</sub> capture tests at Frankfurt Hoechst Industrial Park

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# Background – E.ON Energie's Staudinger 100 kW Pilot Plant

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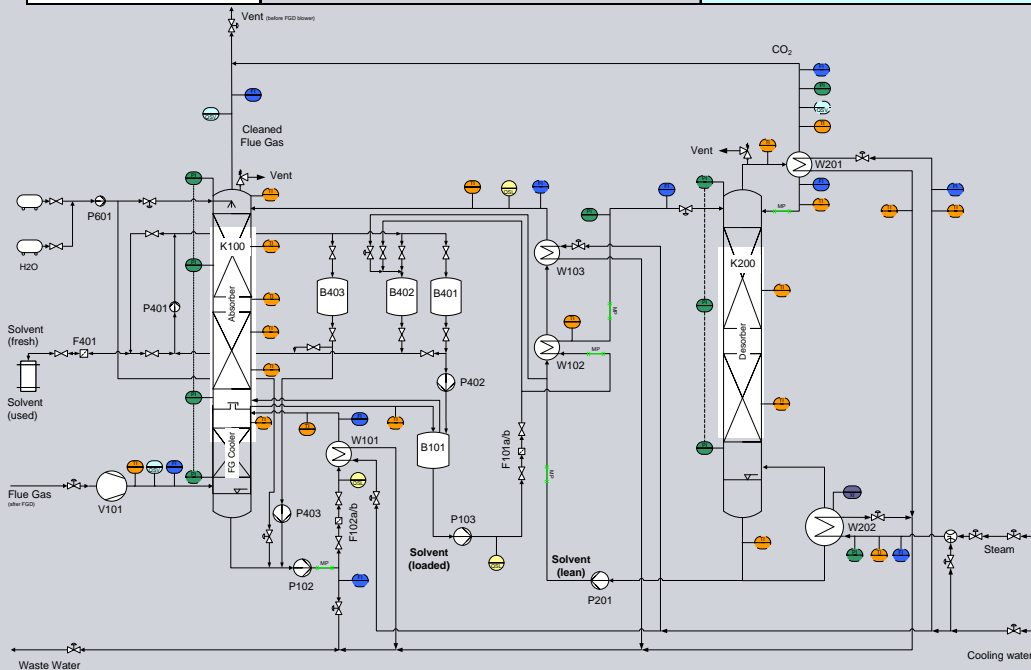
Upscaling via Slip-  
Stream Demopls



# Staudinger Pilot Test Program – 4,500 operating hours as of June 2011

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	2009					2010					
	Q3		Q4			Q1			Q2		
	August	September	October	November	December	January	February	March	April	May	June
Parameter optimization & Model confirmation	Functional tests with H <sub>2</sub> O	Functional tests with solvent				Functional tests with solvent				Further tests	
Stability				Long term test run		Long term test run			Further tests		
Material				Material confirmation Proof of applicability of 1.4571				Material adaptation (Further screening of different materials)			



- Since the start up phase in August 2009 a large amount of test results have been collected
- Test results at different operating conditions were used to validate the existing process model
- Approx. 150 measurements were available to fit the model predictions to reality



# Crystallization

## Absorption capacity

- A high CO<sub>2</sub> loading of the solvent was achieved
- Various SO<sub>x</sub> concentrations can be safely adjusted to investigate the behaviour of active AAS substance



## Crystallization behavior for different solvent concentrations

- Crystallization behaviour as a function of temperature and CO<sub>2</sub> loading was extensively studied and is well understood
- Several process arrangements were made in order to prevent crystallization

Crystallization effects were safely avoided

## Results

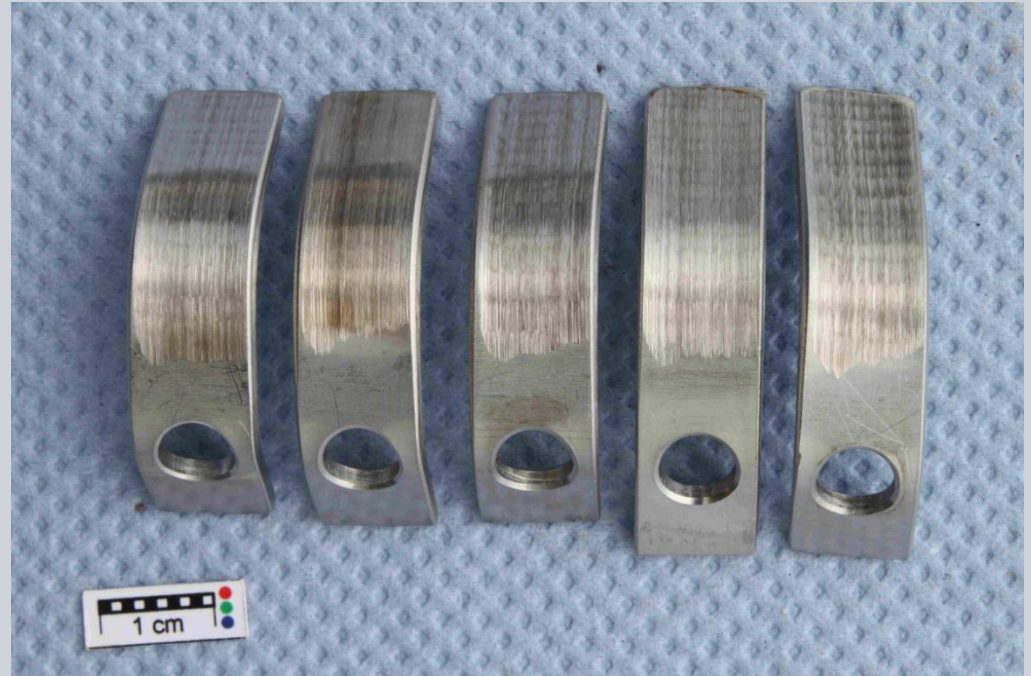
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- the solvent is highly stable and does not lead to measurable loss of active substance due to degradation
- by-products in the liquid phase are salts with no vapor pressure
- No production of any mentionable amounts of emissions
- small amounts of heat stable salts (HSS) and nitrosamines will be removed with a reclaimer

The amino-acid salt is stable against thermal stress and oxygen environments!

# Corrosion Study

- Several Test Coupons (ST 1.4571\*) were investigated from TÜV Süd according DIN 50905
- **No occurrence of local corrosion effects has been observed**
- Similar qualifications have been conducted for lower grade materials (carbon steel 1.0425, st 1.4541, st 1.4525) with generally good results



\*st 1.4571 = EN X6CrNiMoTi17-12-2 or AISI/SAE 316 Ti

Use of material stainless steel 1.4571 was confirmed, good potential for lower grade steels

# Staudinger Pilot Plant Operation Results and Conclusions



## Efficiency

- Low energy consumption
  - < 6% pts efficiency loss
  - 2.7 GJ heat consumption
- High capture rate: >90 % proven

- EU prerequisites can be easily met
- Low CO<sub>2</sub> capture cost

## Emissions

- No predictable solvent and nitrosamine salt emissions

- Add'l washing step avoided
- Permission less critical

## Solvent stability

- < 1%/year solvent degradation by O<sub>2</sub>
- High thermal stability
- Smart reclaimer concept for SO<sub>2</sub> applicable

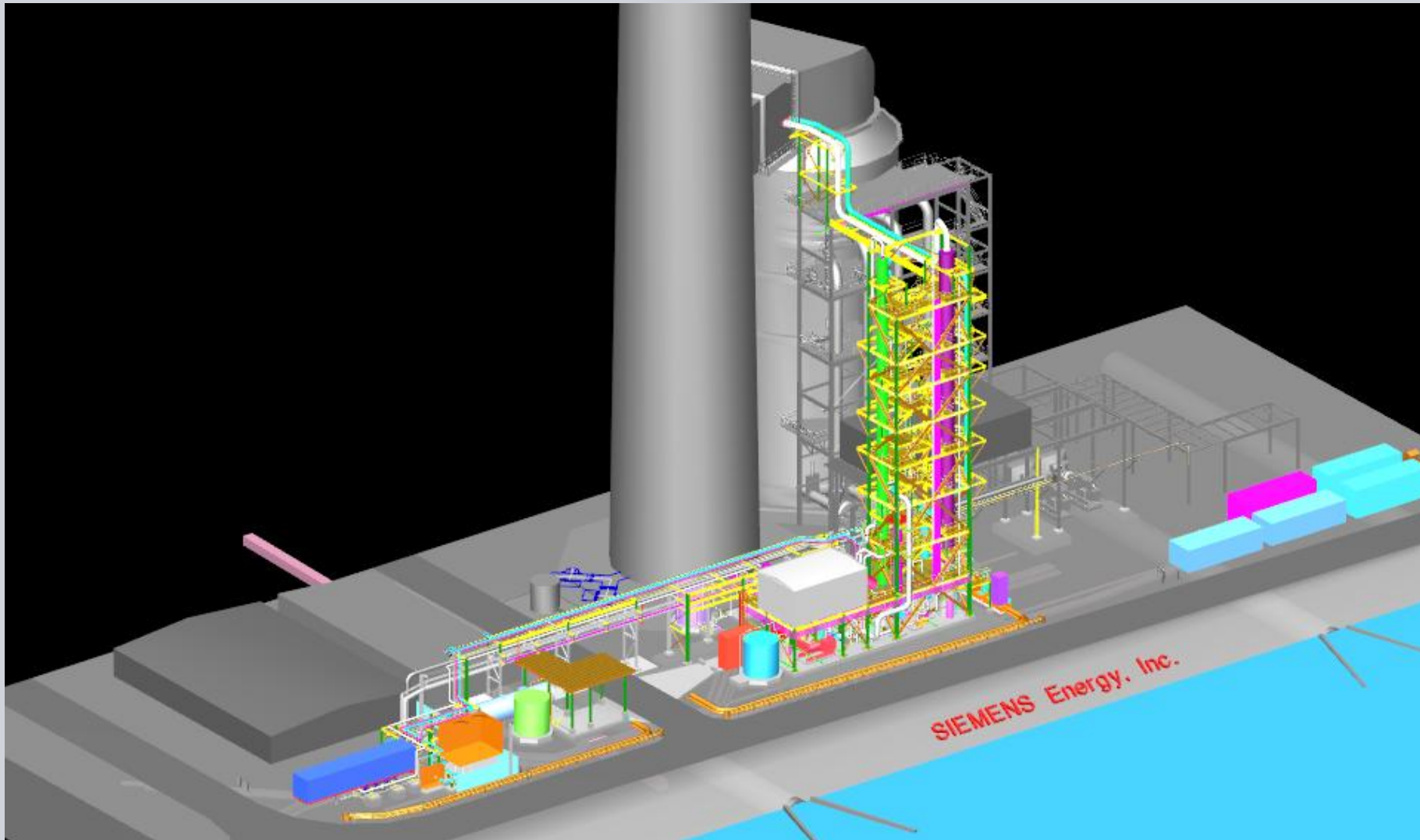
- Low refill requirements
- Low reclaiming costs

## Hardware

- Corrosion tests for construction material in all parts of capture plant

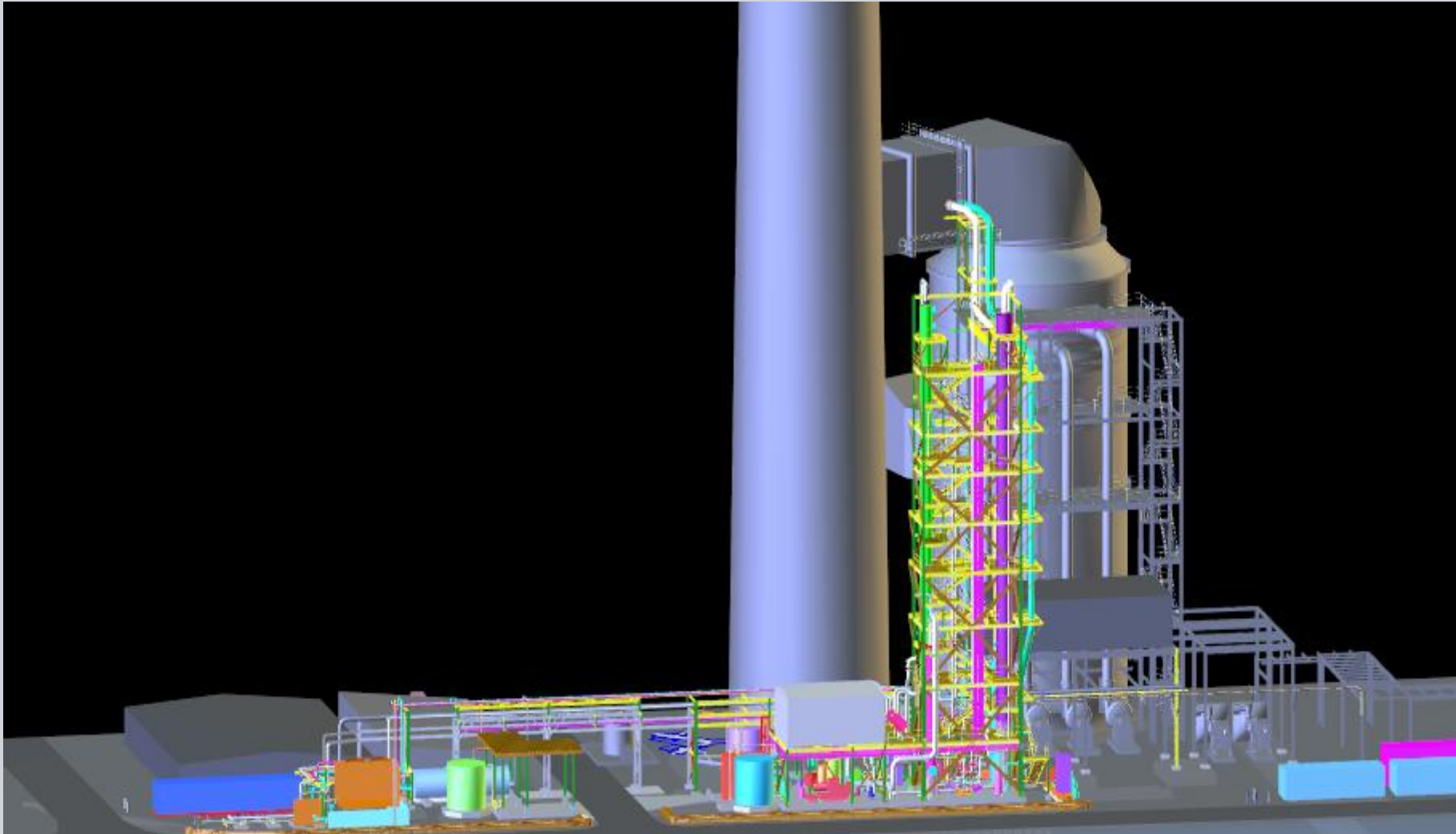
- Standard construction material applicable
- Reduced investment costs

## Current Model Views

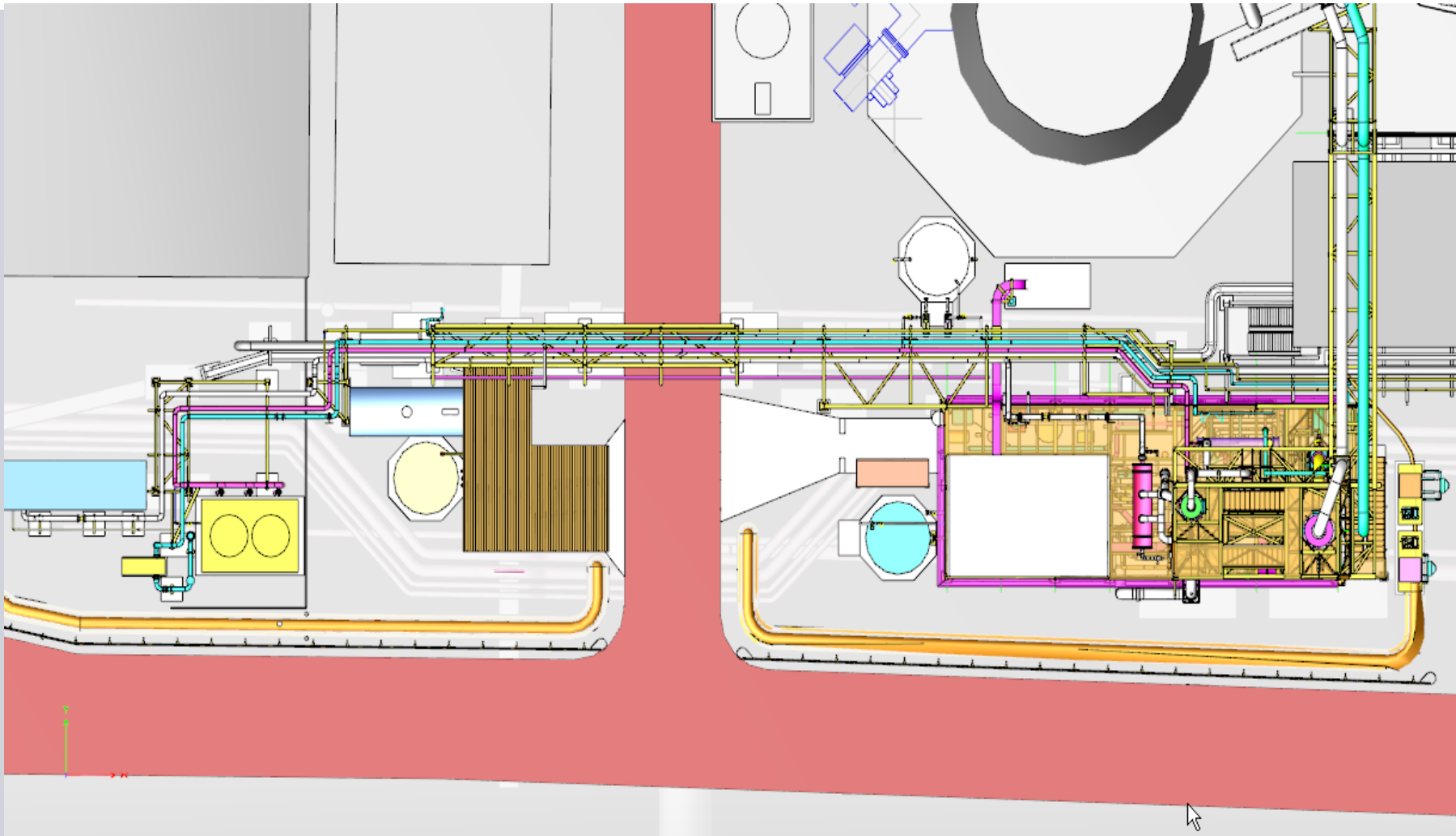




## Current Model Views

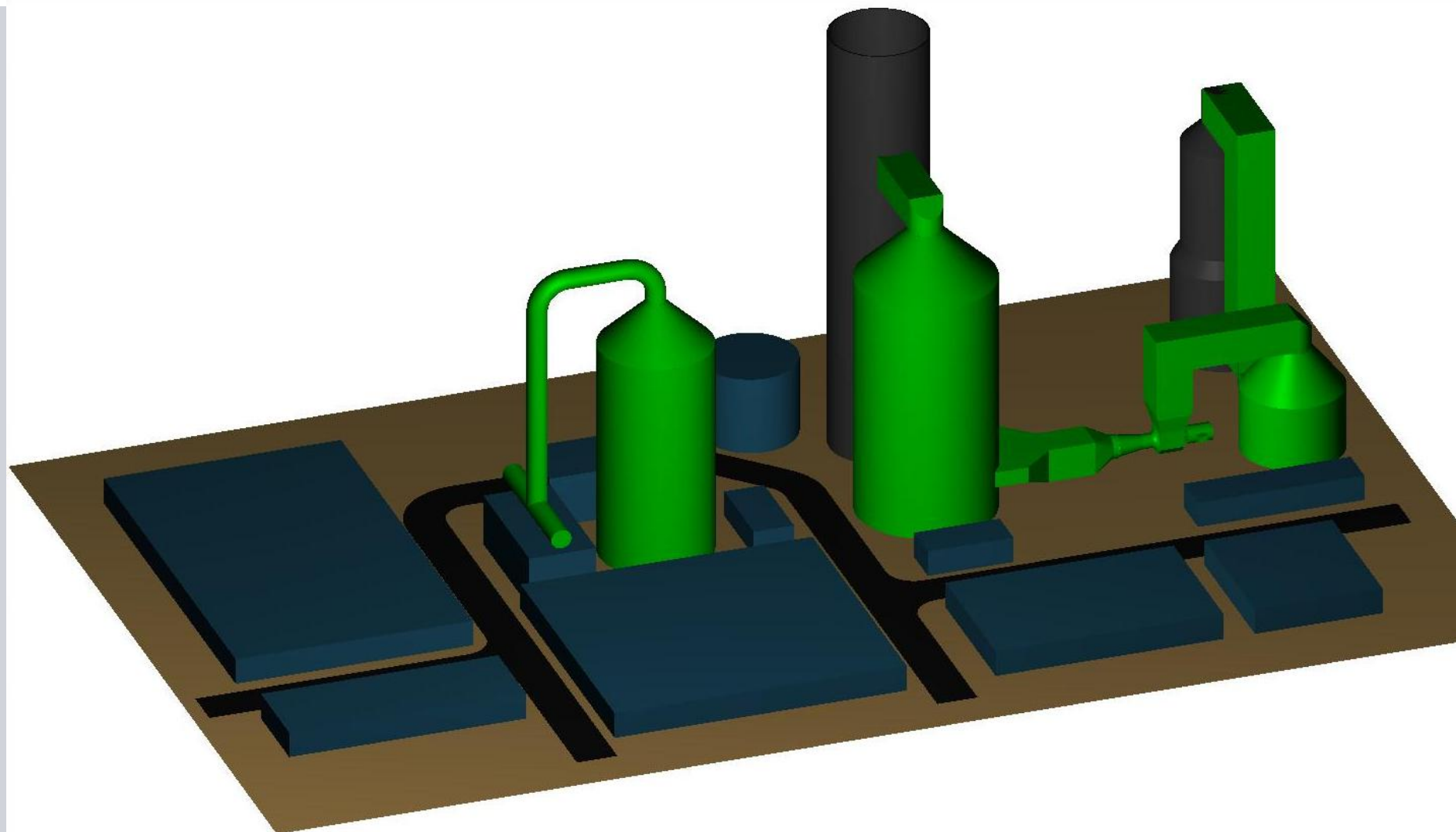


## Current Model Views – Plan at Grade



# Techno-economic Study of PostCap Application 550 MW Utility Plant Case - Model

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## **Industrial Applications**

- **Cement Production**
- **Iron and Steel**
- **IGCC**

## Disclaimer

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